#### Evaluation of the Air-Demand, Flame Height, and Radiation Flux from a Low-Profile Flare

#### Joseph D. Smith, Ph.D. and Ahti Suo-Ahttila, Ph.D.

Alion Science and Technology, Owasso, OK <u>idsmith@alionscience.com</u> - (918) 274-9398

and

#### S. Smith and J. Modi

Zeeco Inc., Broken Arrow, OK

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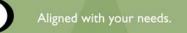




## OUTLINE

Aligned with your needs.

- Introduction to ISIS-3D and Flare Modeling
- ISIS Model Setup and Methodology
- Low Profile Flare Tests
- Model Validation
- Burner Predictions
  - Air Demand
  - Radiation Load
- Observations and Conclusions



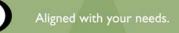
## **ISIS-3D** General Comments

- Based on Computational Fluid Dynamics with radiative heat transfer and combustion chemistry
- Linked model is capable of simulating complex, three-dimensional objects engulfed in fires
- Provides *reasonably* accurate estimates of the total heat transfer to objects from large fires
- Predicts general characteristics of temperature distribution in object
- Accurately assess impact of variety of risk scenarios (wind, % flame coverage, thermal fatigue for given geometry, etc.)
- Reasonable CPU time requirements on "standard" desktop LINUX workstation



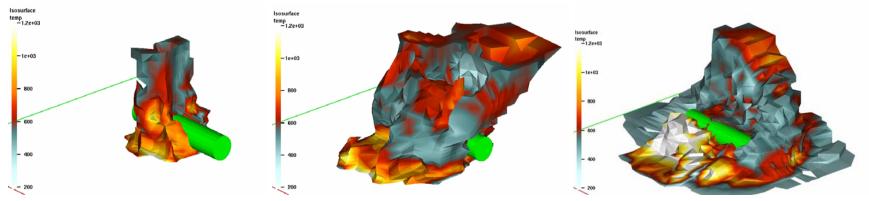
## ISIS-3D Trade-Offs

- Sacrifice generality (large fires only) in favor of quick turnaround time and quantitative accuracy
- Reaction rate and radiation heat transfer models apply only to large fires
- Models intended to make ISIS-3D predictions "goodenough" for industrial use



## **Radiation Inside Large Fires**

- High soot volume fractions make large fires non-transparent (optically thick) which causes flame to radiate as a cloud (radiatively diffuse)
- Fire volume defined as where soot volume fraction is greater than a minimum volume fraction ( $f_{Soot} > f_{min}$ )
- Flame edge (f<sub>FlameEdge</sub>) defined where soot volume fraction is 0.05 ppm
  based on comparisons with large fire experiments



Calculated flame surfaces for 3 time steps from ISIS-3D simulation of validation experiment



## Radiation Outside of Large Fires

- When  $f_{Soot} < f_{FlameEdge} =>$  outside "flame" (participating medium considered)
- View factors from fire to un-engulfed surfaces calculated at each time step (include attenuation by flames)
- Radiation view factor from object surface to surroundings calculated at each time step
- $\mathcal{E}_{\text{FireSurface}} = I$  (fire is black body radiator)
- Radiation from fire surface to surroundings based on  $T_{surround}$  = Constant



## **Diffuse Radiation Within Fire**

• Calculated indirectly using a Rossland effective thermal conductivity

$$k_R = \frac{16\sigma T^3}{3\beta_R} >> k_{Air}$$

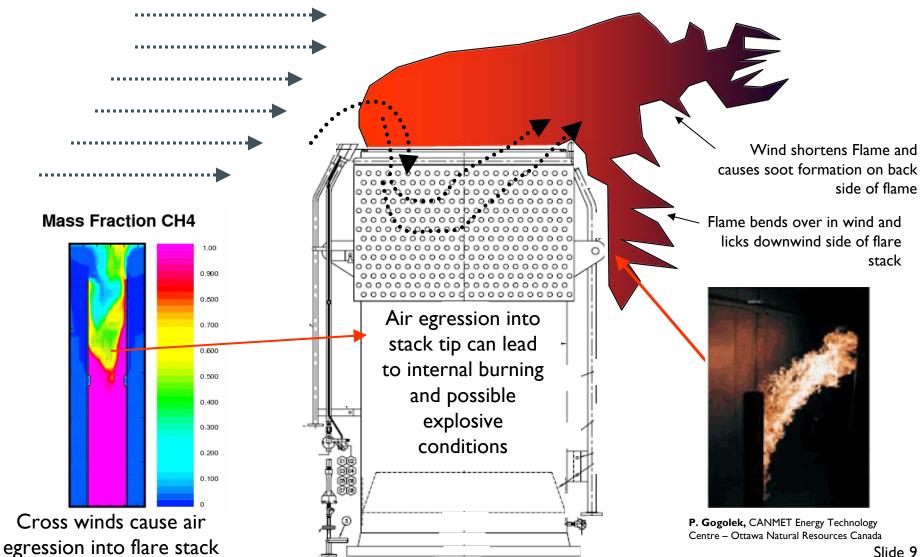
- $\sigma$  = Stefan-Boltzman Constant
- T = Local temperature
- $\beta_R$  = Local extinction coefficient (dependent on local species concentrations)



## Combustion Model

- Variant of Said et al. (1997) turbulent flame model
- Relevant Species (model includes relevant reactions)
  - F = Fuel Vapor (from evaporation or flare tip)
  - O<sub>2</sub> = Oxygen
  - $PC = H_20(v) + CO_2$
  - C = Radiating Carbon Soot
  - IS = Non-radiating Intermediate Species
- Eddy dissipation effects and local equivalence ratio effects
- Reactions based on Arrhenius kinetics
- C and T<sub>A</sub> determined for all reactions

#### Flares in Cross Winds - Modeling Issues

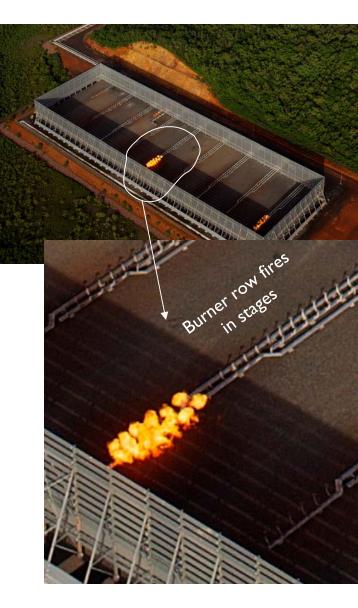


#### Low Profile Flares - Modeling Issues

- High tip velocity increases air entrainment
  - Tip design critical to air entrainment
  - Local high velocity can translate into high sound levels
- Assist media not available to increase combustion air
  - smoke below certain tip pressure (D-stage pressure)
- Tip spacing critical

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- Flares must cross light
- Possible Flame merge lengthens flames
- Adjacent rows compete for air (longer flames, poor performance)



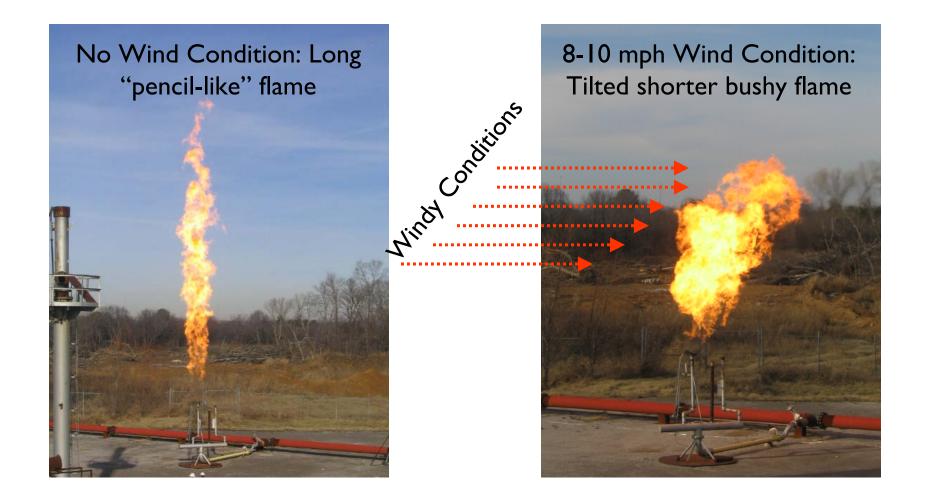


## Approach to Modeling Full Flare Fields

- Model Single Burner Test
  - Perform Calibration Tests
  - Calibrate Soot Yield and Reaction Parameters for Test Fuel
  - Predict flame shape and size
- Model Multi-Burner Test
  - Perform Radiation Calibration Tests
  - Check Tip/Row Spacing
  - Predict flame shape and size
- Model Full Flare Field
  - Use Calibrated Soot Yield and Radiation Models
  - Predict Flare Performance (Smoke Production/Air Demand)
  - Predict Radiation Load on Wind Fence



#### Single Tip Burning Propane: wind vs. no-wind





## Modeling Low Profile Flare Test

- Propane injected as mass, momentum and species sources
- Fuel Mol wt 44 ( $C_3H_8$ )
- Tip elevation 2.0 m (6.5 ft)
- Tip Geometry Provided by Client
- Test Conditions for Propane Mass Flow = 0.46 kg/s (3,651 #/hr)
- Flame height determined by fuel and soot burnout
- Air inflow calculated implicitly from pressure boundary conditions
- Radiation Flux calibrated from measured data at two locations



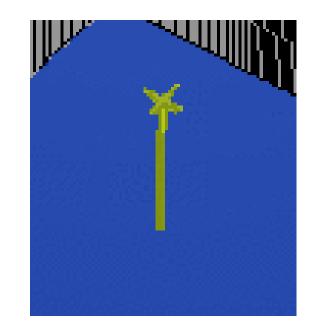
#### Single Burner Flare Model

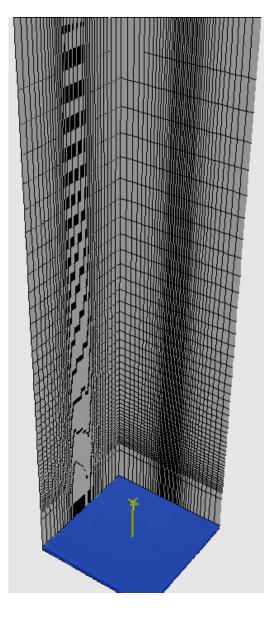
- 6 x 6 x 26 m physical domain
- Flare tip located 2 m above ground level
- Turbulence and Arrhenius kinetics Included for fuel gas
  - Reaction Parameters adjusted to match observed flame characteristics
  - Soot Yield matched flame height (i.e., soot burnout)
- Flare Movies for no wind, 3m/s (7mph) wind conditions
- Predicted results for Air demand and Radiation loss from flame determined

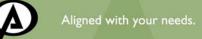


## Single-burner Mesh

- Rectangular cells
- Local refinement near burner tip
- > 110,000 computational cells







#### Combustion Models

#### Propane:

C<sub>3</sub>H<sub>8</sub> + 3.6 O<sub>2</sub> → 3 CO<sub>2</sub> + 1.6 H<sub>2</sub>O + 0.024 Soot + 46 MJ/kg propane Soot + 2.66 O<sub>2</sub> → 3.66 CO<sub>2</sub> + 32 MJ/kg Soot

#### Ethylene:

 $C_2H_4 + 0.57 O_2 \rightarrow 0.93 C_2H_2 + 0.64 H_2O + 9.4 MJ/kg ethylene$  $C_2H_2 + 2.58 O_2 \rightarrow 2.7 CO_2 + 0.7 H_2O + 0.2 Soot + 34.1 MJ/kg intermediate$ Soot + 2.66 O<sub>2</sub> → 3.66 CO<sub>2</sub> + 32MJ/kg Soot

#### Mixed Gas:

 $0.572 C_2H_4 + 0.383 C_2H_6 + 0.043 H_2 + 0.982 O_2 \rightarrow$ 

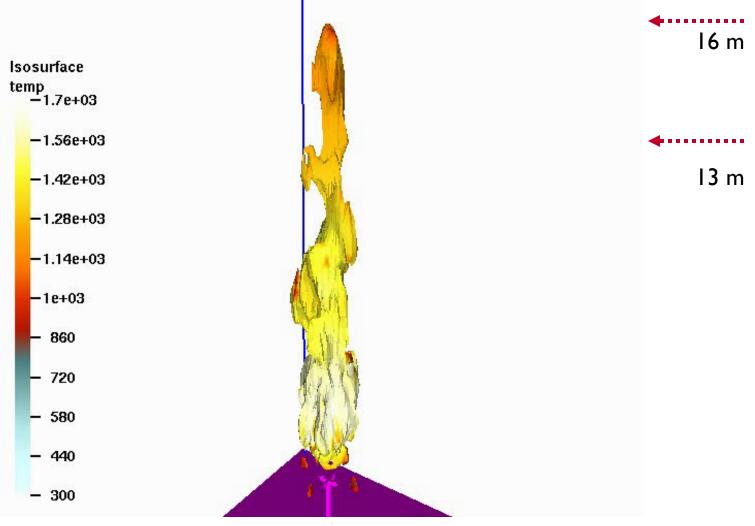
0.53 C<sub>2</sub>H<sub>2</sub> + 0.34 C<sub>2</sub>H<sub>3</sub> + 1.1 H<sub>2</sub>O + 14.2 MJ/kg

0.61 C<sub>2</sub>H<sub>2</sub> + 0.39 C<sub>2</sub>H<sub>3</sub> + 2.66 O<sub>2</sub> →

2.66 CO<sub>2</sub> + 0.813 H<sub>2</sub>O + 0.181 Soot + 34.4 MJ/kg

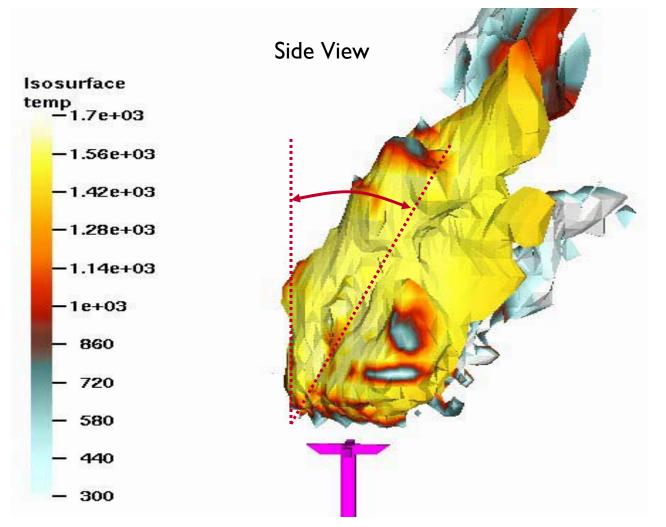
Soot + 2.66 O<sub>2</sub> → 3.66 CO<sub>2</sub> + 32 MJ/kg

#### Flame in No Wind

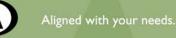


No wind produces tight "pencil-like" flame

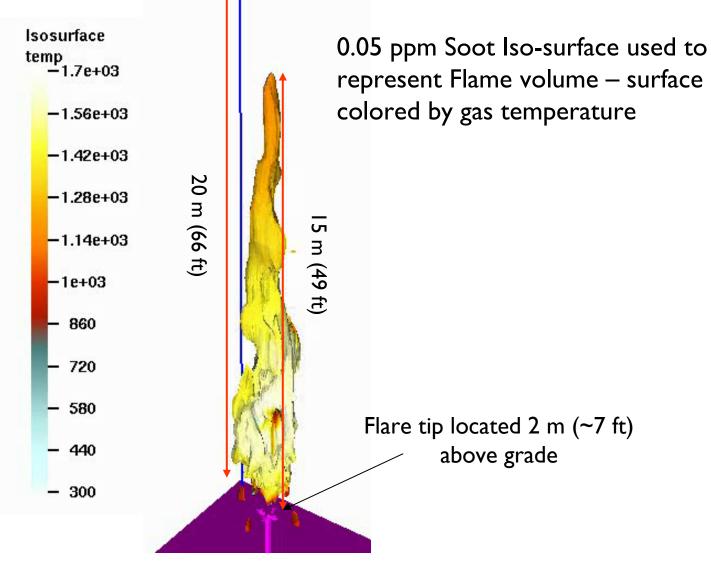
## Flame in 3.0 m/s Wind



Wind produces tilted bushy, shortened flame

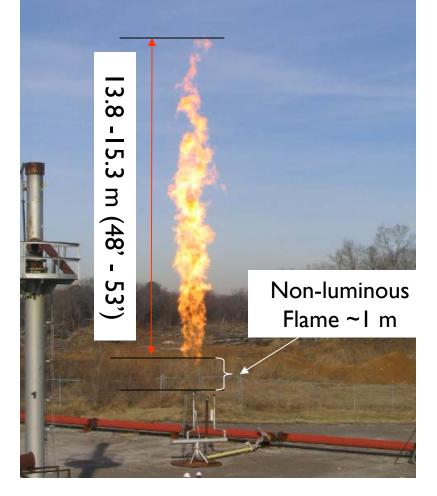


#### Predicted flame length for no-wind condition

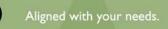


#### Single-Tip Ground Flare Test Results

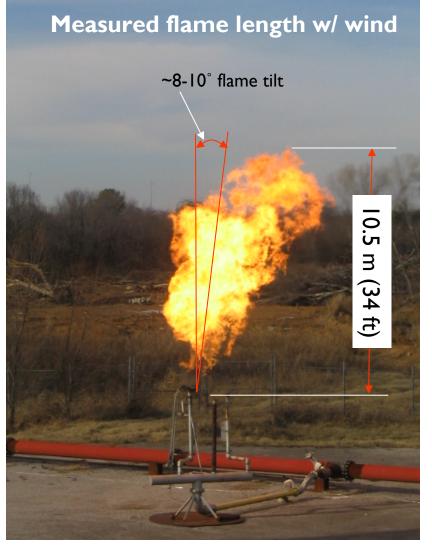
#### Measured flame length wo/ wind



- No Wind Condition (<I mph wind)
- Ave Flame Length = 14.8 16.3 m (48 53 ft)
- "Pencil-like" tight flame
- Small non-luminous flame at base
- Propane Flow rate: measured 1.4" WC @ 57 °F across orifice plate => 7.3 psig tip back pressure (measured on 18 inch pipe run)



#### Single-Tip Ground Flare Test Results

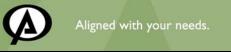


- I.4" WC @ 57 °F => 7.3 psig tip pressure
- I2-I6 Km/hr (8-I0 mph) crosswind
- ~30% flame height reduction
- Minimum flame tilt (~8°)

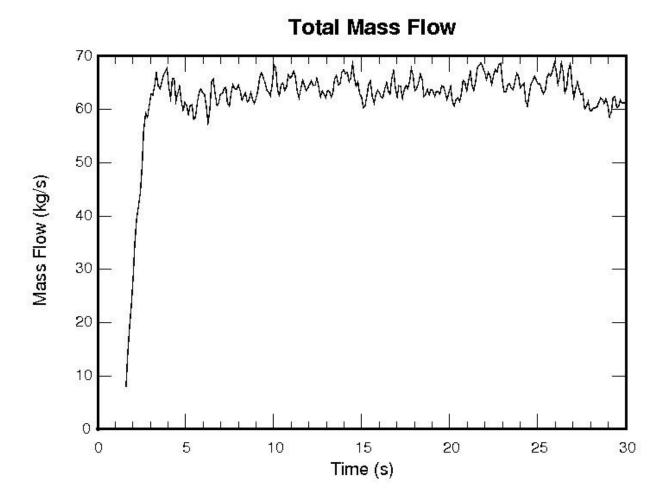


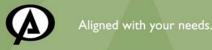
#### Model Used to Predict Flare Air Demand

- Based upon total mass flow through a 3.6 m square plane located
  20 m height above flare
- Predicted flame height is 17 m above ground (15 m flame length)
- Predicted 60 kg/sec air demand by flame
- Total air inflow through all walls around computational domain is 100 kg/sec



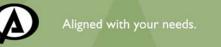
#### Predicted Air Demand vs. Time



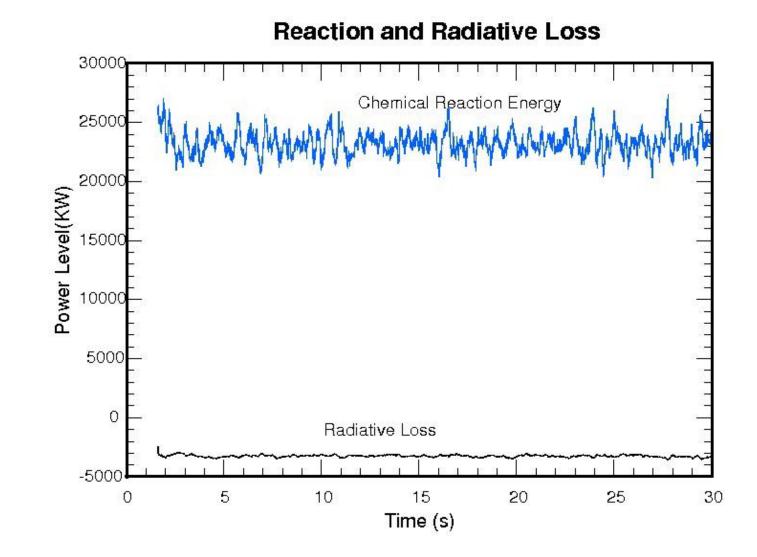


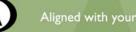
#### Model Used to Predict Flame Radiation Loss

- Radiation Depends upon Soot, CO<sub>2</sub>, H<sub>2</sub>O Concentration in Flame and Flame Size
- Soot yield from hydrocarbon assumed constant for propane
- Predicted approx 3 MW radiation loss from 22 MW Flame or 13.6% heat loss



#### **Predicted Flame Energy Balance**

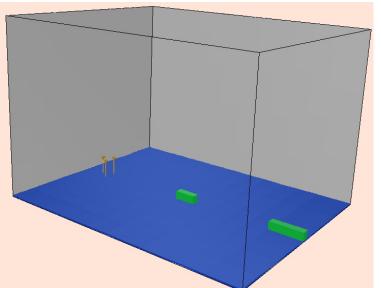


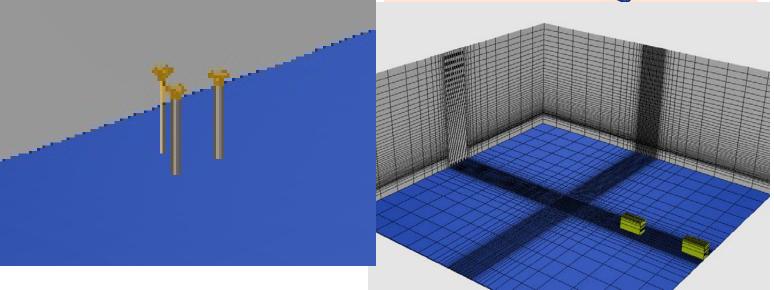


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#### **Three-burner Mesh**

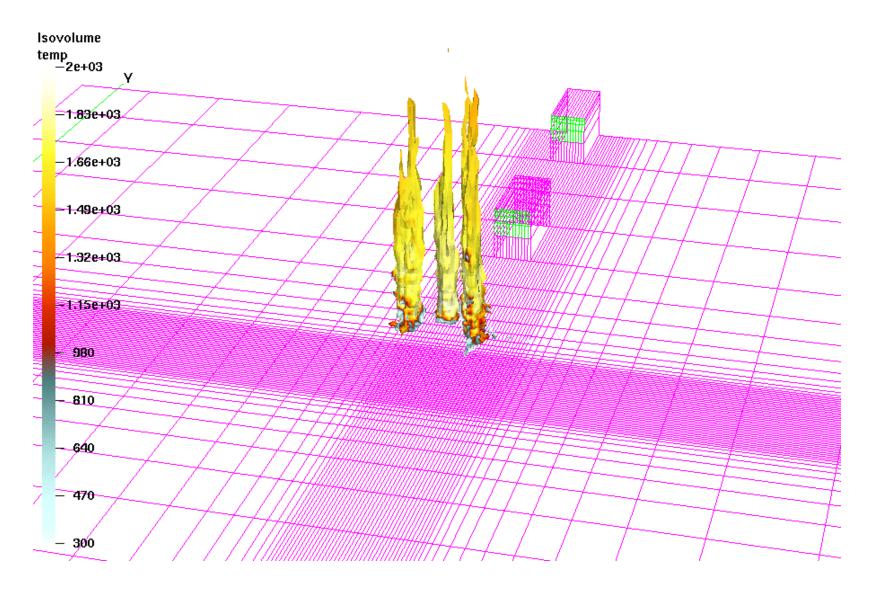
- $\succ$  Rectangular cells
- $\succ$  Domain size is 30 m X 35 m X 25 m
- Local refinement near burner tips and radiation meters
- > 188,000 computational cells



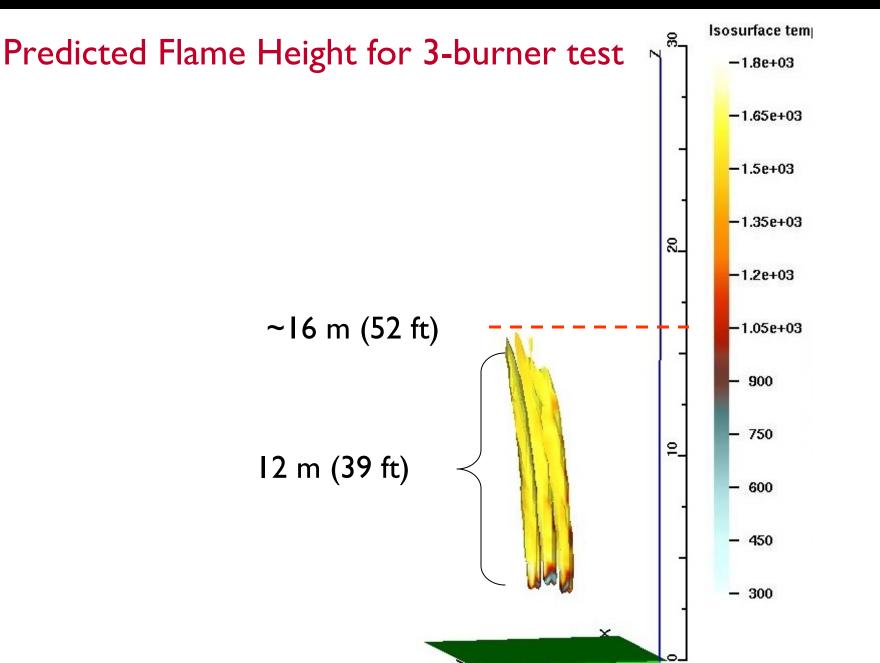




#### Predicted 3-burner flare with radiation monitors



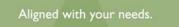
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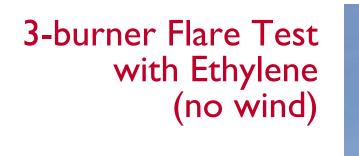


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Flame height ~I I m (~36')

Non-luminous region ~1 m (3')

Tip Height~3 m (10')



#### Predicted Radiation from 3-Burner Flare after Modifications to Account for Ground and Atmospheric Attenuation Effects

Radiation Issues Accounted for in Prediction:

- Ground re-radiating and reflecting incident radiation from flame to flux meters Ι.
  - $\geq$ Assumed ground  $\varepsilon = \alpha = 1$ ; allow ground to heat to steady state temperature
- Atmospheric attenuation of radiation from flame to flux meters 2.
  - $\geq$ Model uses ambient/source temperatures with  $H_2O/CO_2$  absorption

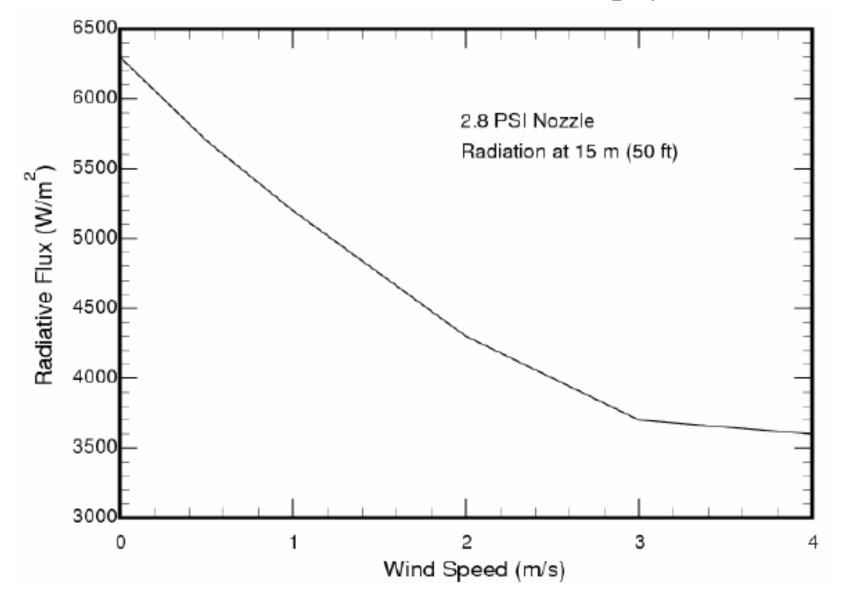
WALL (from plan view perspective)	Left Wall ISIS-3D Output" W/m <sup>2</sup>	Right Wall ISIS-3D Output W/m <sup>2</sup>	Bottom Wall ISIS-3D Output W/m <sup>2</sup>	Flame Optical Thickness
PEAK FLOW				
<b>Initial Radiation</b>	78,000	63,000	108,000	0.275
<b>Radiation Modification</b>	61,000	35,000	NA	
SUSTAINED FLOW				
<b>Initial Radiation</b>	15,000	15,000	35,000	0.28
<b>Radiation Modification</b>	6,600	6,600	NA	

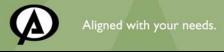
# 3-Burner Flare Radiation Predictions Compared to Experimental Data

Tip	Position	Burner Pressure	Total Predicted Radiation	Measured Radiation	Difference
Size	(m)	(psi)	(W/m²)	(W/m²)	(%)
3	15	2.8	2700	3344	-20.0 %
3	15	7.3	4750	4803	-1.0 %
3	15	11.4	6150	6192	-0.7 %
3	30	2.8	650	671	-3.0 %
3	30	7.3	1350	1184	+14.0 %
3	30	11.4	1650	1532	+8.0 %
4	15	2.8	4325	6371	-32.0 %
4	15	7.3	8050	8192	-2.0 %
4	15	11.4	10000	9536	+5.0 %
4	30	2.8	1150	1513	-23.0 %
4	30	7.3	2580	2464	+5.0 %
4	30	11.4	3250	2747	+18.0 %

#### Wind Effect on Radiative Flux from 3-burner $C_2H_4$ flare at 15 m

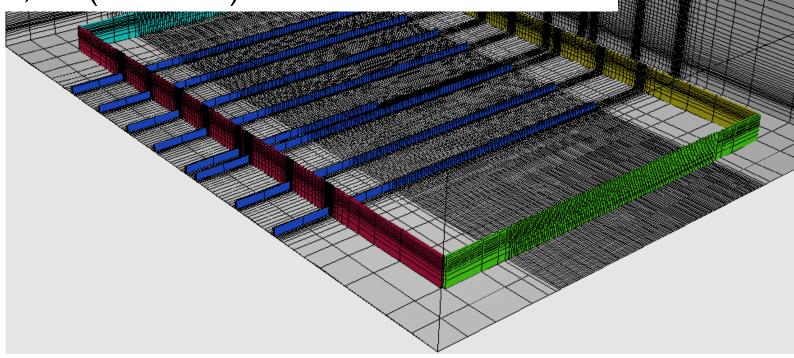
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## Full Field Flare Grid

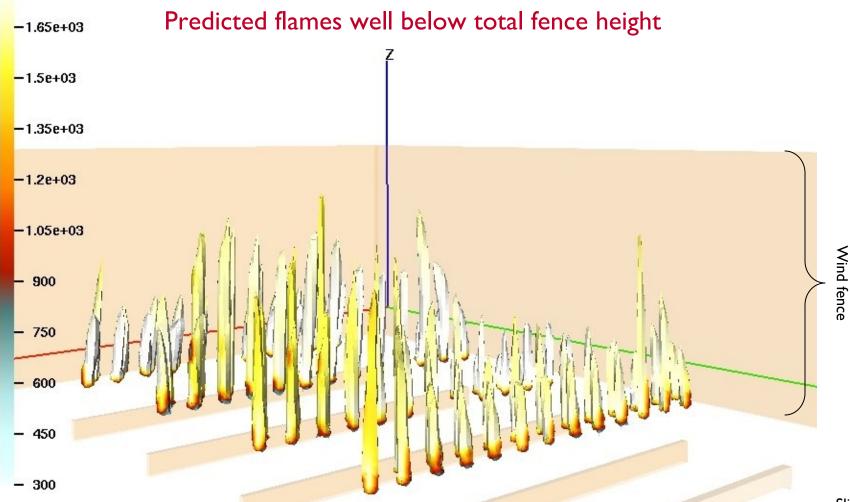
- Domain size is 10 m beyond wind fence and 25 m high
- Local refinement near burner rows/tips
- > 700,000 (Sustained Flow)
- > 1,200,000 (Peak Flow)





#### [C<sub>2</sub>H<sub>4</sub>] Iso-surface for 1/4 Symmetry Peak Flow-no wind condition

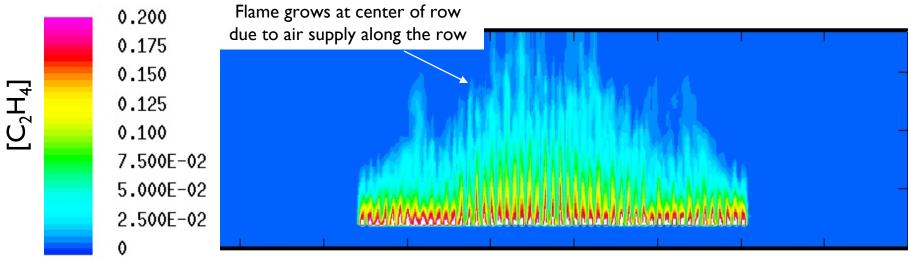




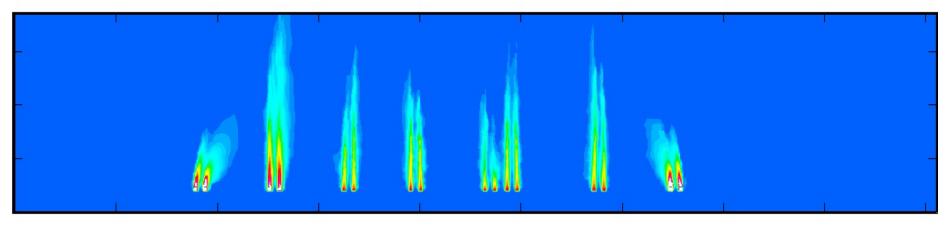


#### Max $[C_2H_4]$ along line of sight for peak flow case

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Side view along row showing flame elongation toward center of row



End view of flame height for each row and impact of inflow on outer rows



#### Summary of all Air/Fuel Requirements for "no-wind" conditions

Case Description	Evaluation Plane Area (m <sup>2</sup> )	Total Air Flow (kg/s)	Fuel Flow (kg/s)	Air/Fuel Mass Ratio
1 Burner Propane	14.63	60	0.46	130
1 Burner (Tip 3) Ethylene	13.26	52	0.94	55
3 Burner (Tip 3 - 7.3PSI) Ethylene	36	134	2.88	47
3 Burner (Tip 3 - 11.4PSI) Ethylene	36	144	3.84	38
3 Burner (Tip 4 - 7.3PSI) Ethylene	36	150	4.26	35
3 Burner (Tip 4 - 11.4PSI) Ethylene	36	160	5.79	28
Full Field Peak Flow Ethylene	3226	9700	262.3	37
Full Field Sustained Flow Mixed Gas	1843	4800	93.6	51.3



### **Conclusions**

- ISIS-3D Model:
  - > Single-burner model used 110,000 cells
  - > Three-burner model used 188,000 cells
  - > Full-field model used 700,000 cells (Sustained Flow);
  - > 1,200,000 cell (Peak Flow)
  - > Combustion chemistry for propane, ethylene, mixed gas
- Modeled flame shape/size for 3 fuels for single and three burner tests
- Predictions compared to data from 12 tests (2 tip sizes, 3 operating pressures, 2 radiation sample locations)
- Predicted "reasonable" estimates of radiation heat transfer and air demand for low profile flare
  - > Air/fuel ratios range from 28 to 47 for 3-burner test and from 37 (Peak Flow Case) to 51 (Sustained Flow Case)
- Calibrated flare model applied to full-flare field to estimate:
  - > Air demand for specified tip/row spacing
  - > Radiation load on wind fence for nominal and peak flow cases
  - > Expected flame height and smoke production for nominal and peak flow cases