

# A Mechanistic Investigation of Nitrogen Evolution and Corrosion with Oxy-fuel Combustion

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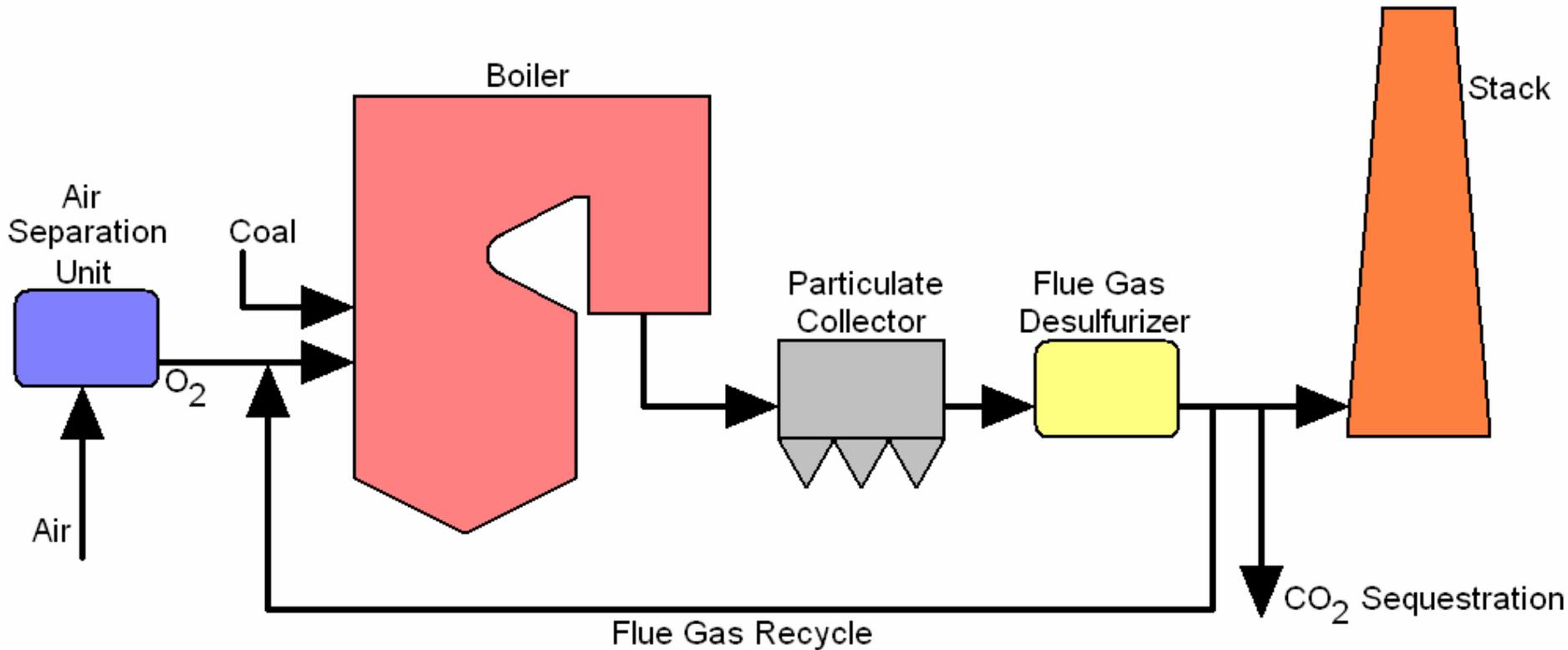


# Introduction: NO<sub>x</sub> Formation

- Thermal NO<sub>x</sub> – slowest forming, requires high T
- Prompt NO<sub>x</sub> – quicker forming but slower than other combustion reactions
- Fuel-NO<sub>x</sub> – like prompt-NO but N originates from fuel
  - Most of NO<sub>x</sub> from coal combustion is fuel-NO<sub>x</sub> (80%)

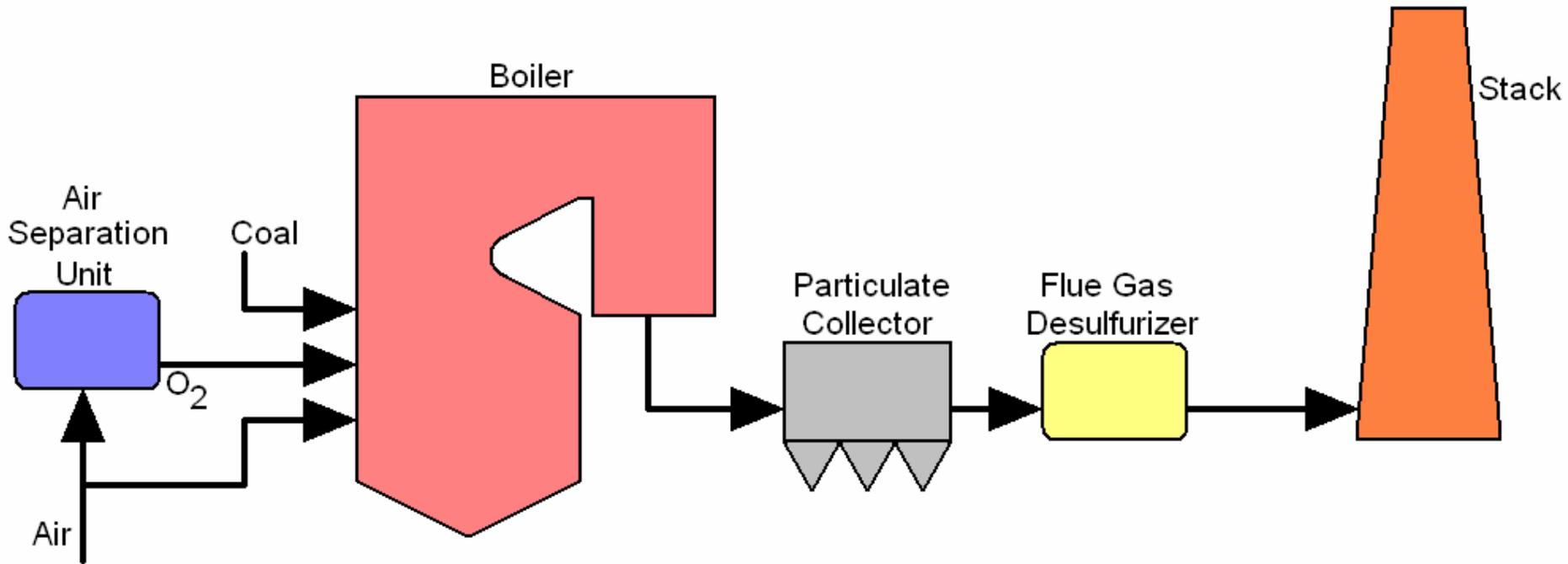


# Introduction: pc Oxy-fuel Combustion



**O<sub>2</sub> Volume %: ~30%**

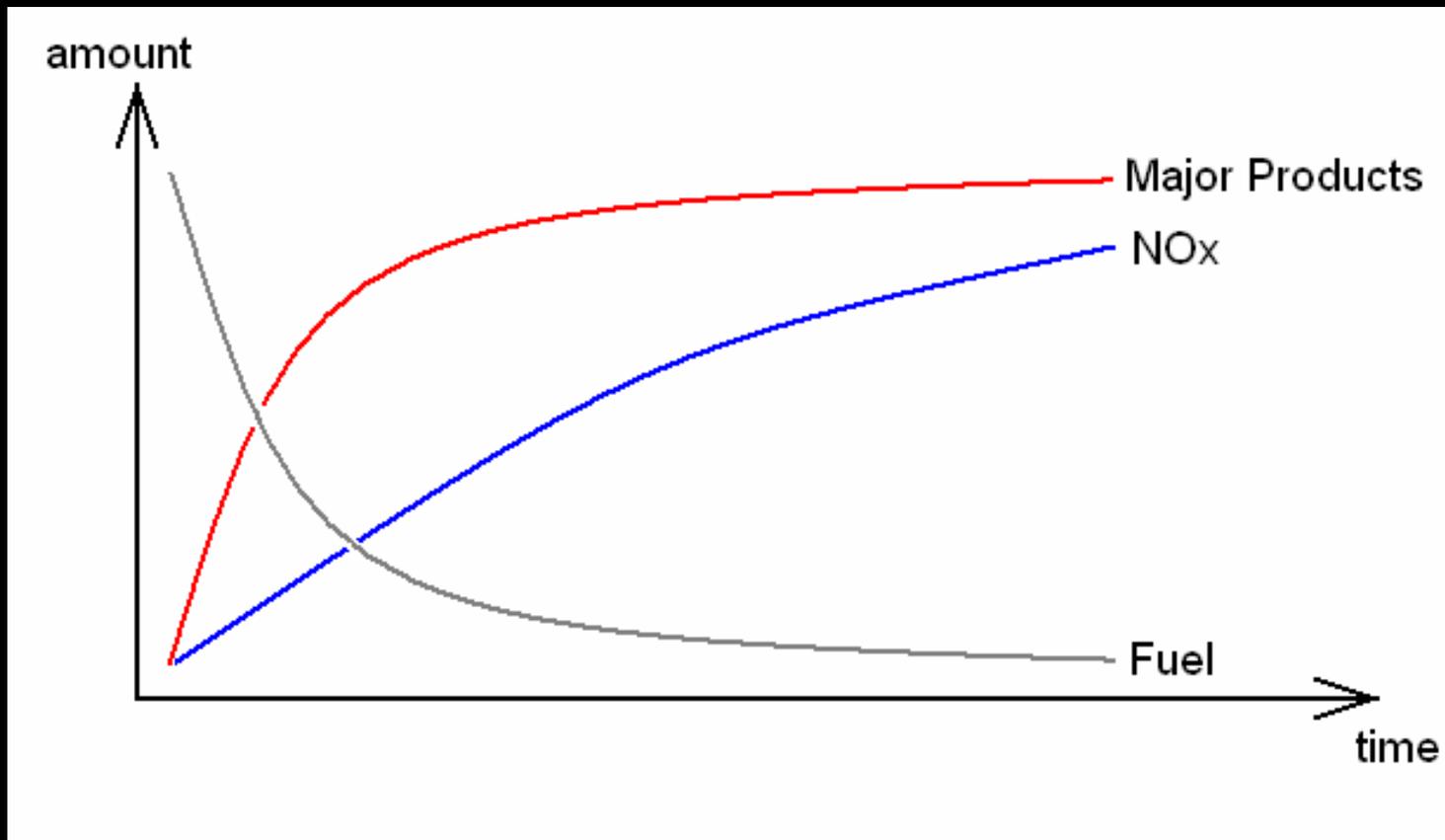
# Introduction: pc O<sub>2</sub> Enhanced Combustion (OEC)



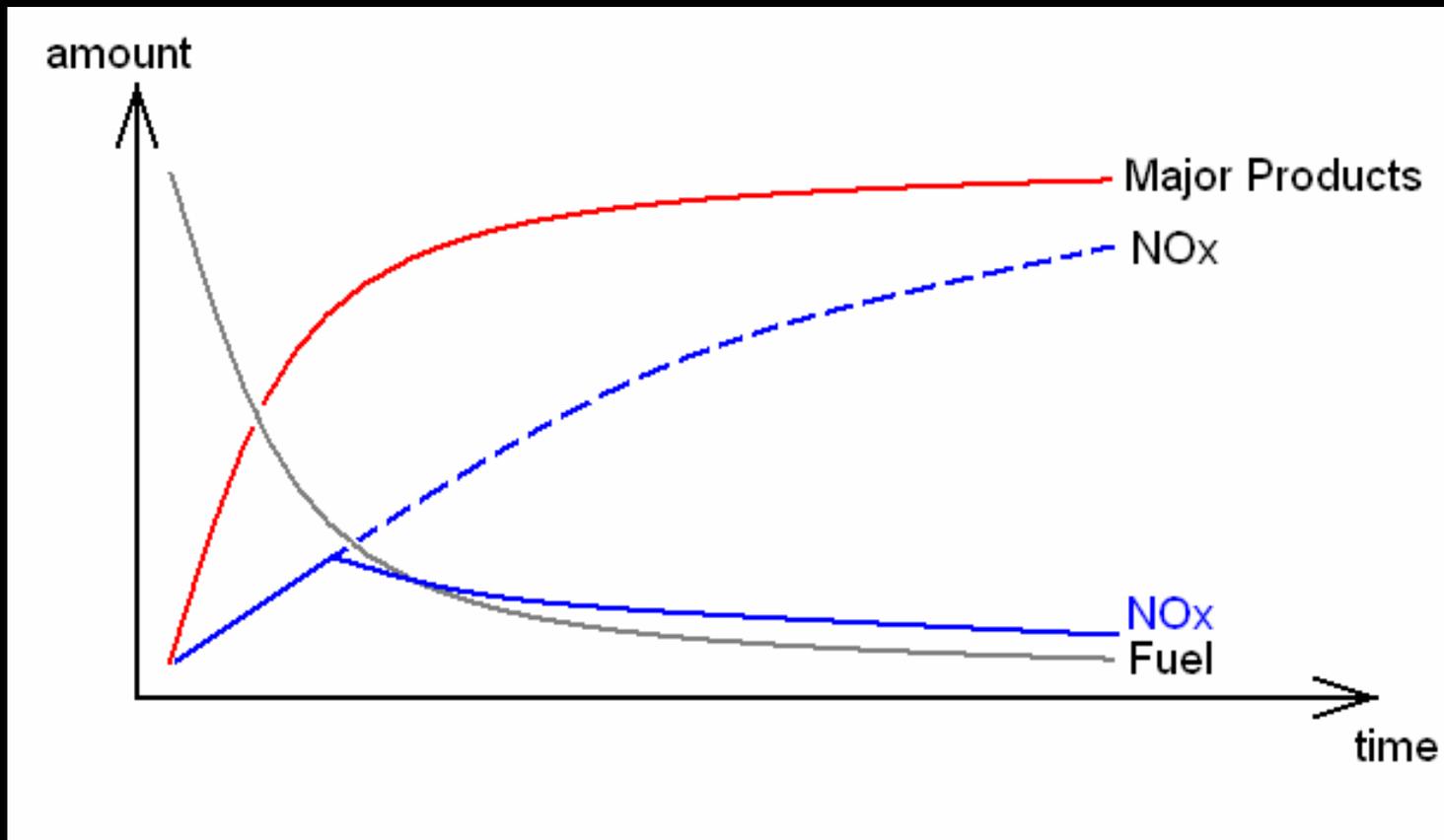
**O<sub>2</sub> Volume %: 21.8 to 29% (in a fuel-rich stage only)**

(US Patent # 6,957,955 Kobayashi, et al., 2005)

# Oxygen Enhanced Combustion



# Oxygen Enhanced Combustion



# OEC and Oxy-fuel $\text{NO}_x$ Comparison

Expected Common Features (relative to air):

- Higher  $\text{O}_2$  concentration in fuel-rich region leads to:
  - Higher volatiles yield (lower char-N)
  - Shorter devolatilization period
  - Attached/Stable flame
- Longer residence times in fuel-rich zone:
  - More  $\text{NO}_x$  can be reduced
- Optimization is required



# Introduction:

## OEC and Oxy-fuel $\text{NO}_x$ Comparison

### Differences:

- OEC has (relative to Oxy-fuel):
  - High sensitivity to  $\text{O}_2$  injection location
  - Large amounts of  $\text{N}_2$  (possibility of thermal and prompt  $\text{NO}_x$ )
- Only Oxy-fuel has:
  - Flue gas recycle (including  $\text{NO}_x$ )
  - Replacement of almost all  $\text{N}_2$  with  $\text{CO}_2$
- Increased concentrations of corrosive species

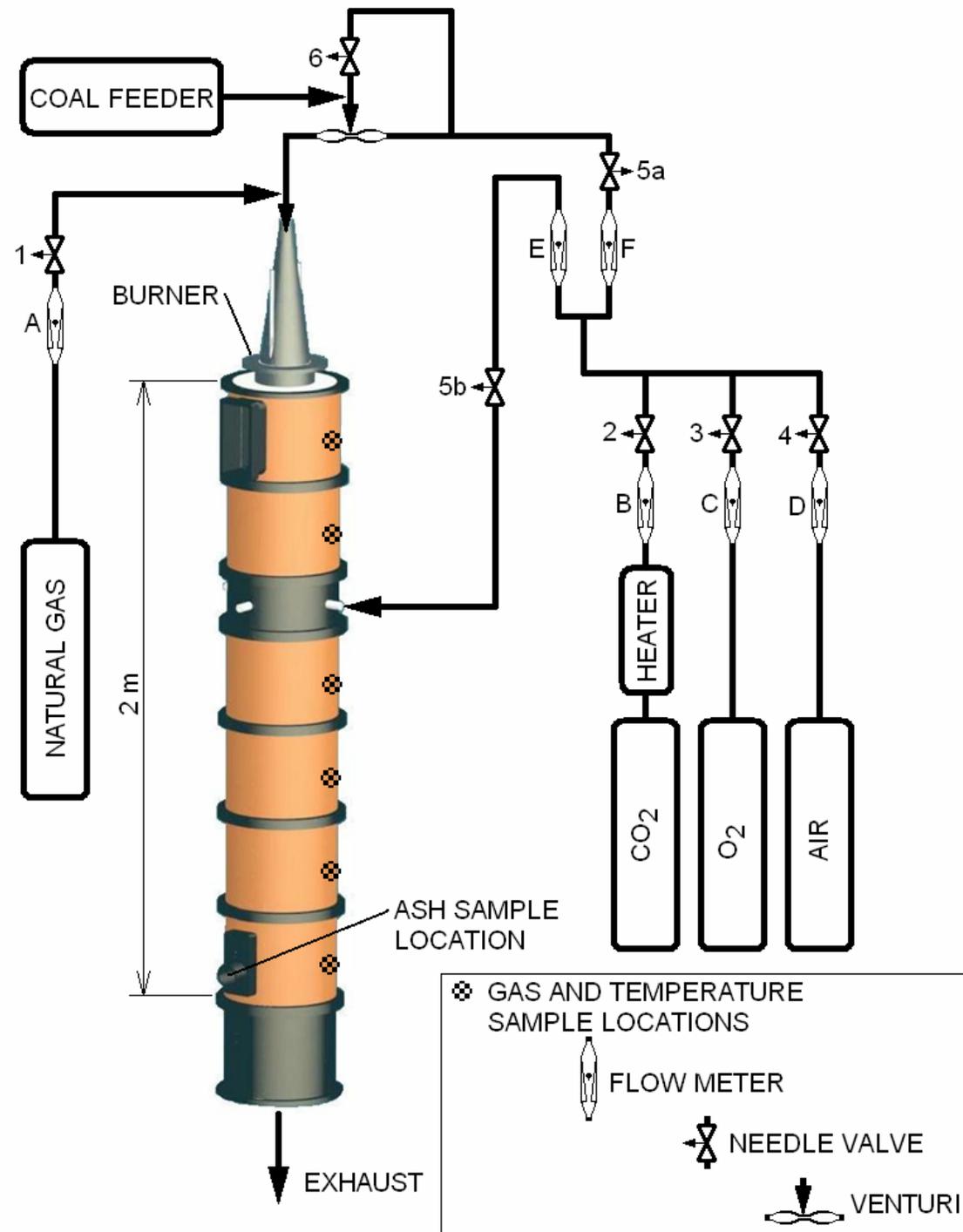


# Objectives

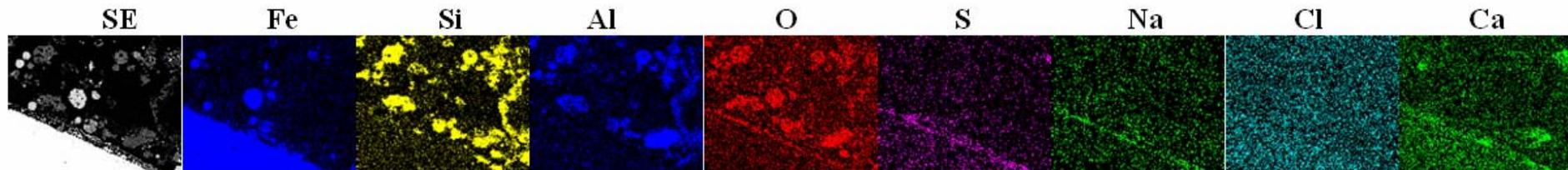
- Understand the mechanism(s) by which  $\text{NO}_x$  emissions are lowered in oxy-fuel combustion
  - leads to ability to optimize the process
- Measure indicators of corrosion tendency for oxy-fuel combustion relative to air



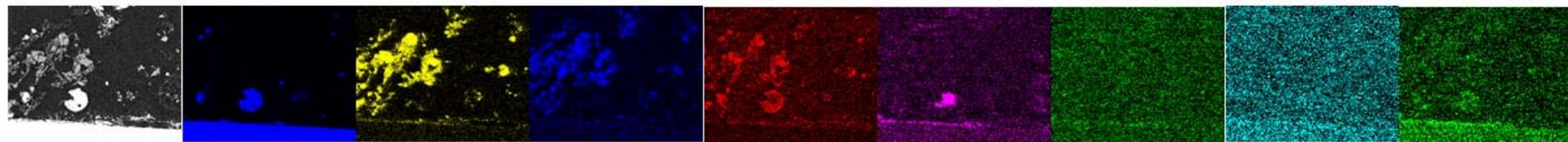
# Equipment Setup



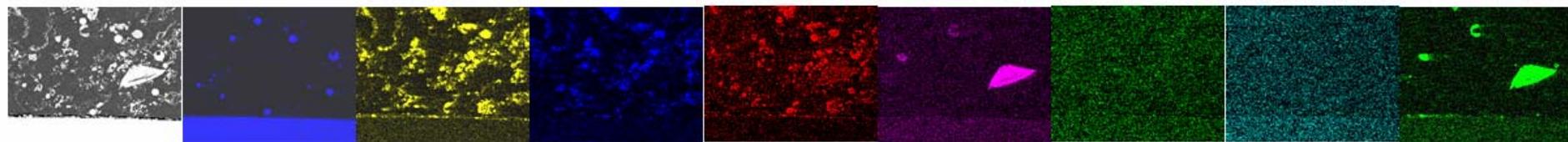
# Preliminary Corrosion Results



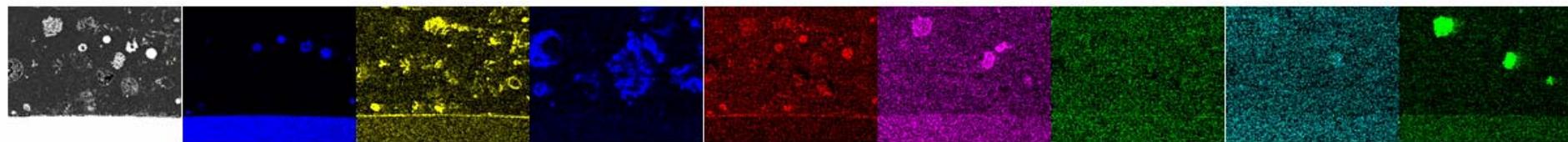
Illinois #6 (Normal) Magnification – 500X



Illinois #6 (Oxyfuel) Magnification – 400X



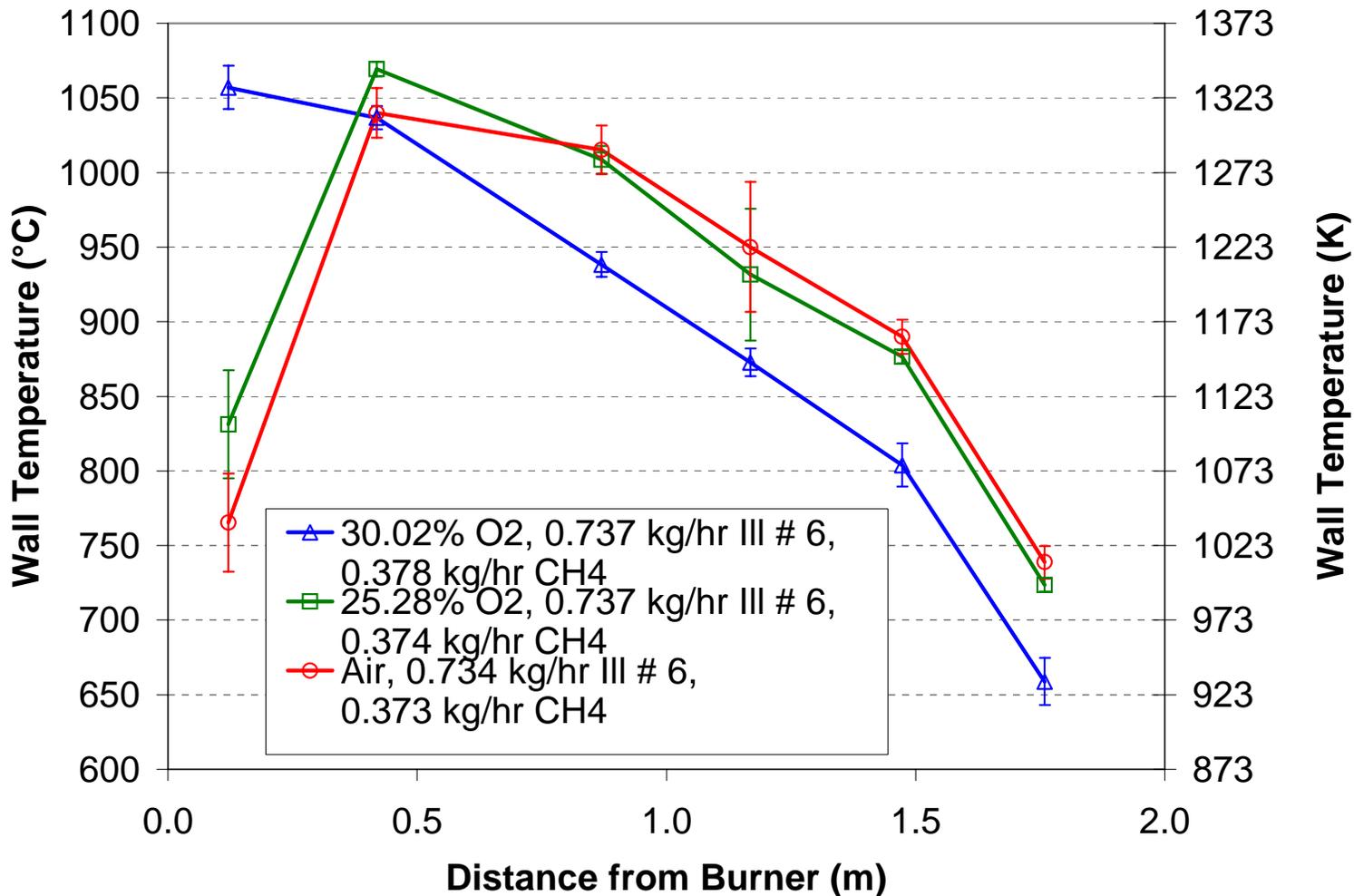
Illinois #6 (Normal) Magnification – 268X



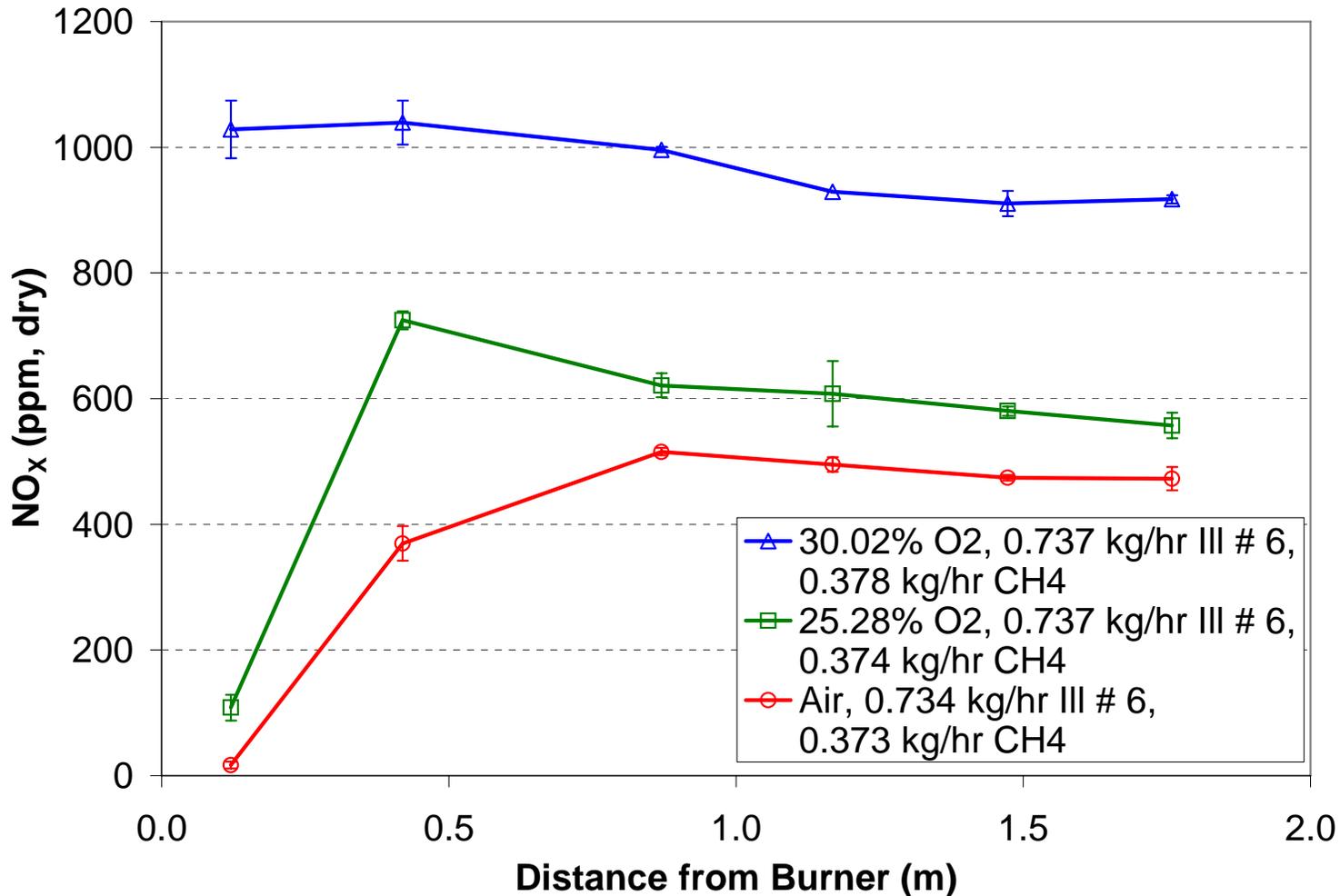
Illinois #6 (Oxyfuel) Magnification – 200X



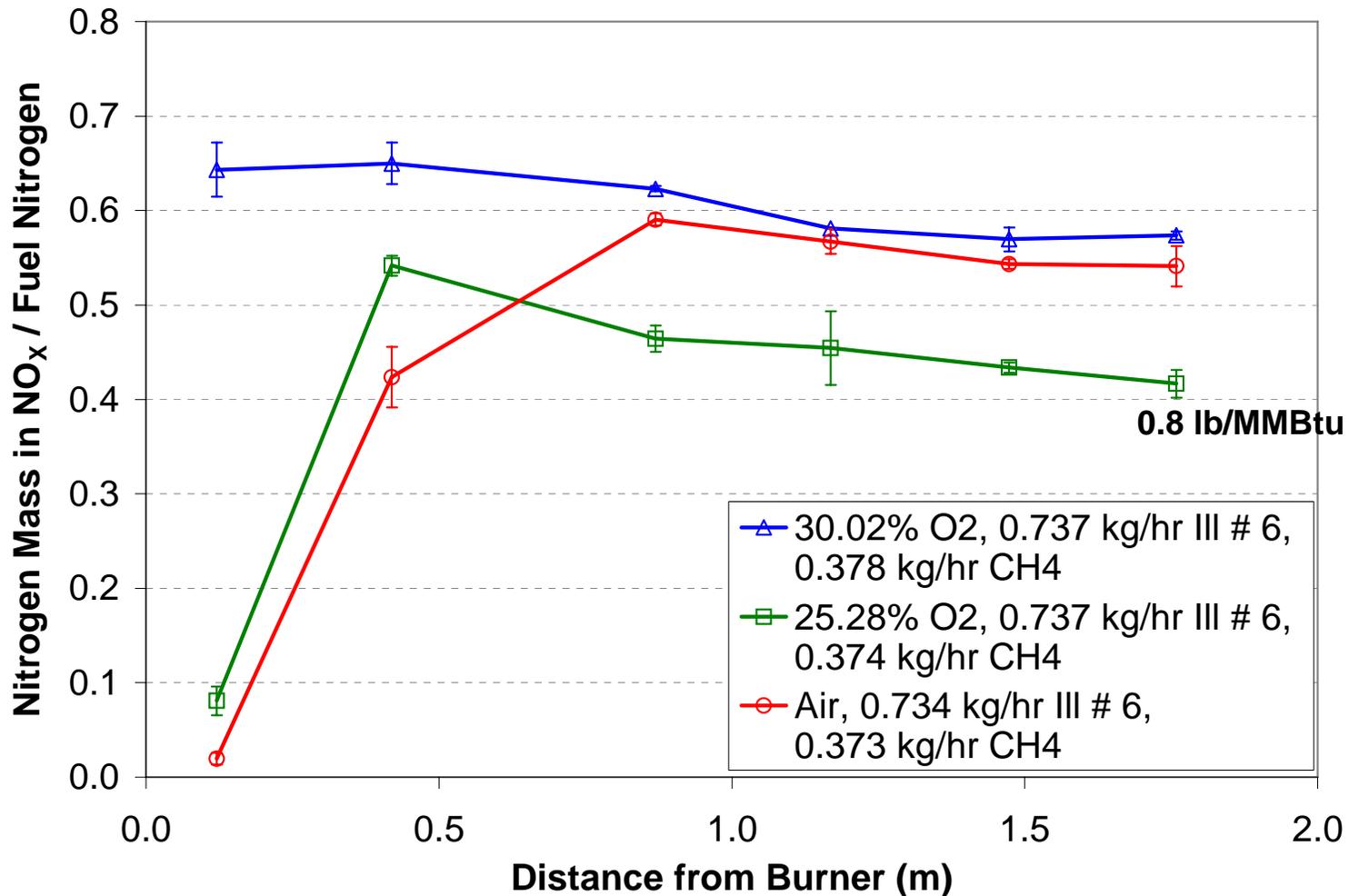
# NO<sub>x</sub> Results: Unstaged



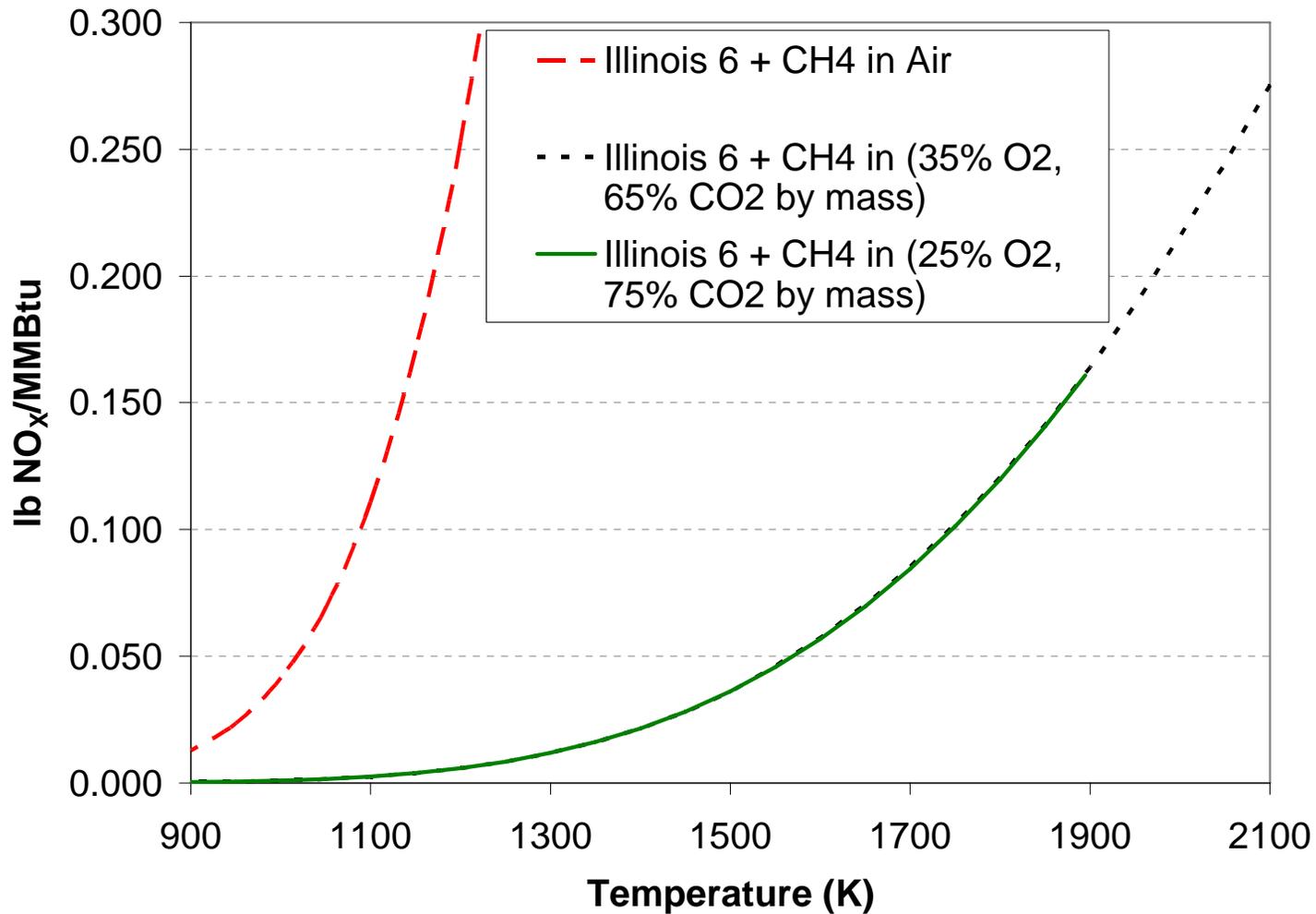
# NO<sub>x</sub> Results: Unstaged



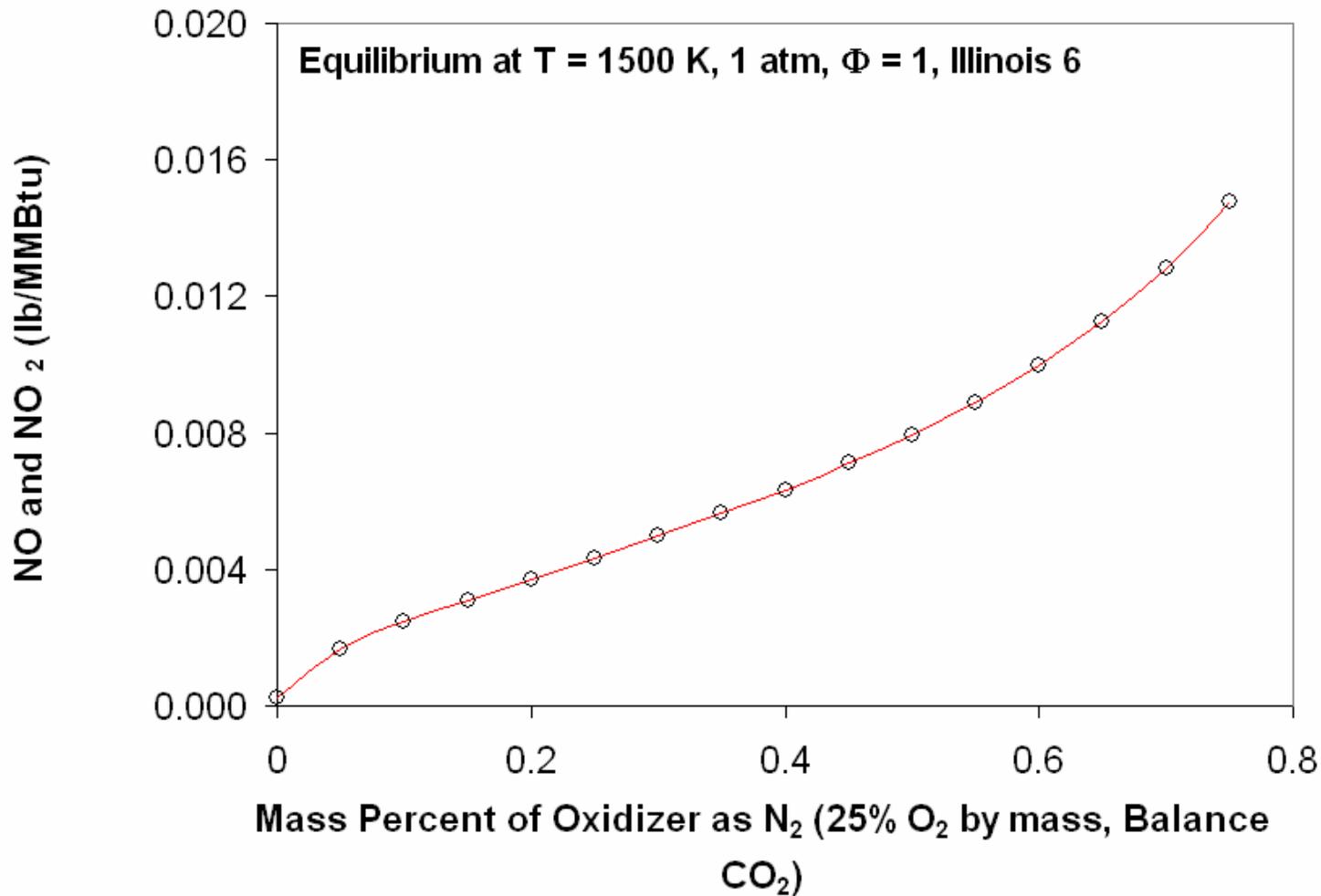
# NO<sub>x</sub> Results: Unstaged



# Equilibrium $\text{NO}_x$ Trends



# Equilibrium $\text{NO}_x$ Trends



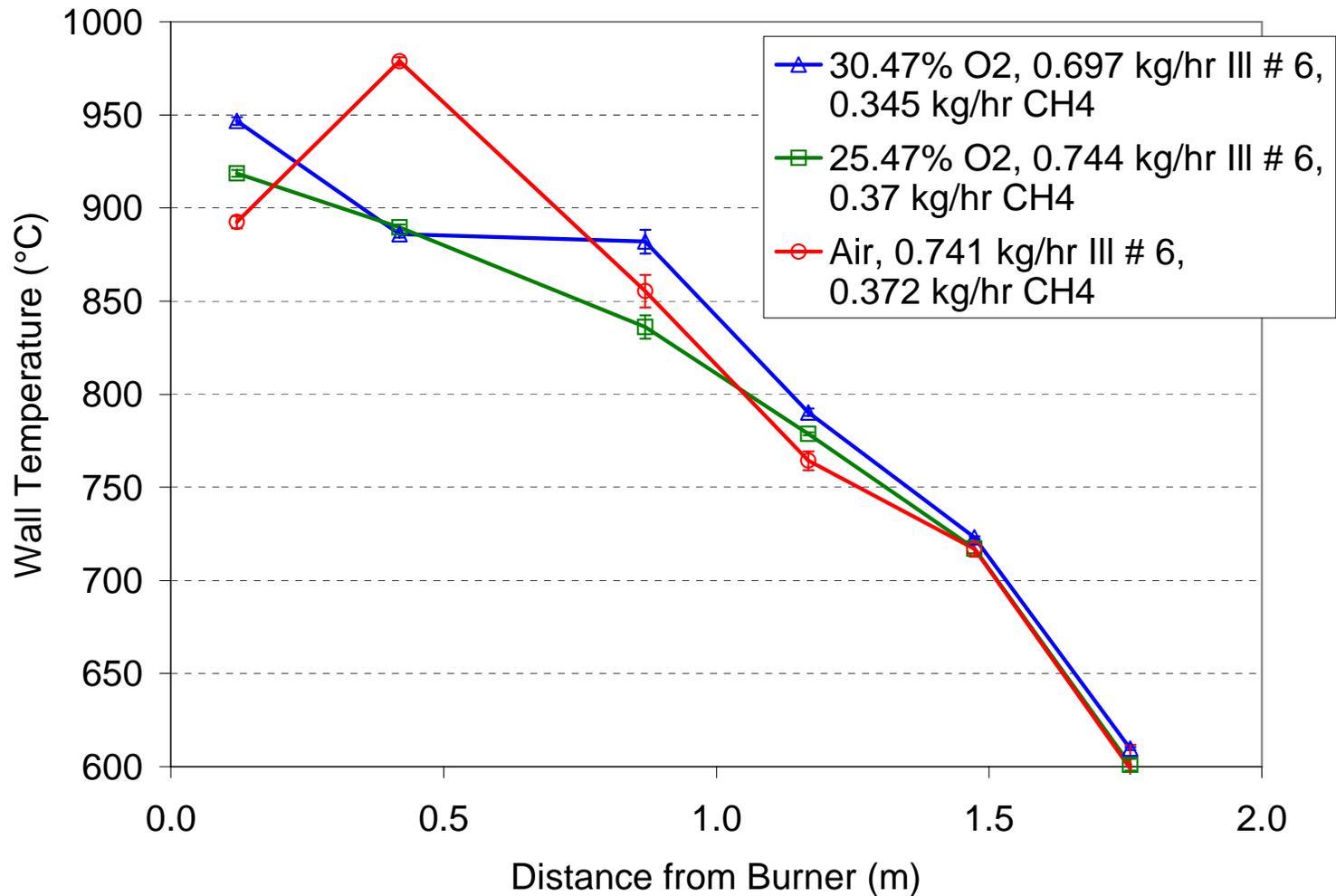
# NO<sub>x</sub> Results: Staged



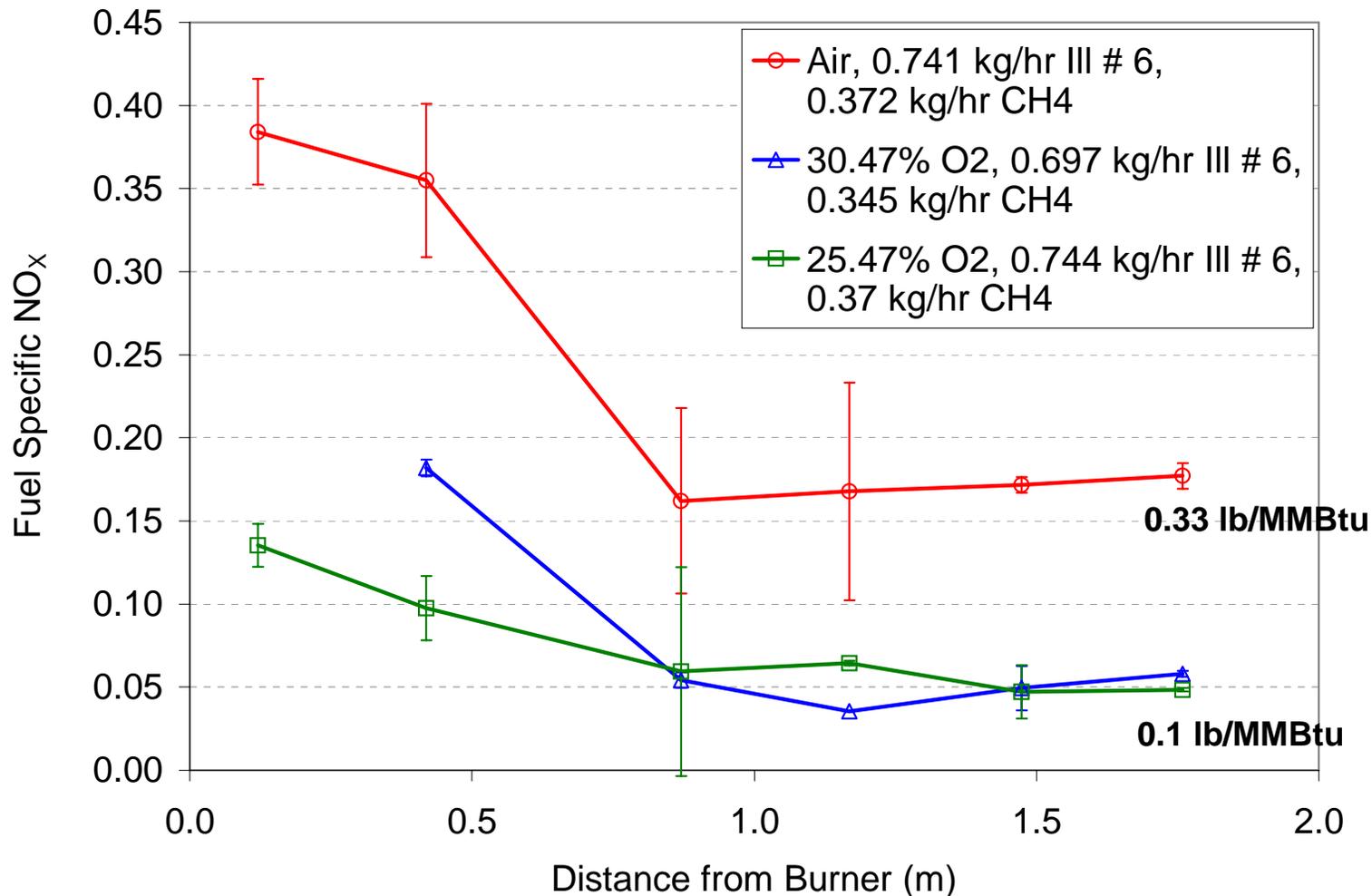
Total Mass Flow Rates (kg/hr)					Stoichiometry				
Coal	CH <sub>4</sub>	Air	O <sub>2</sub>	CO <sub>2</sub>	Oxidizer to Burnout Section	Primary Stage SR	Sec. Stage SR	Oxidizer Mass % O <sub>2</sub>	Oxidizer Molar % O <sub>2</sub>
0.741	0.372	16.8	-	-	28%	0.75	1.05	23.3%	21%
0.744	0.370	-	3.886	11.37	28%	0.75	1.04	25.5%	32%
0.697	0.345	-	3.562	8.127	28%	0.73	1.02	30.5%	38%



# NO<sub>x</sub> Results: Staged



# NO<sub>x</sub> Results: Staged



# Summary

- Without staging, Oxy-fuel and Air combustion produce  $\text{NO}_x$  in large amounts
- With staging, Oxy-fuel produces lower  $\text{NO}_x$ 
  - BUT: Recycle ratio must be optimized
    - Affects peak  $\text{NO}_x$  formation
    - Affects residence time

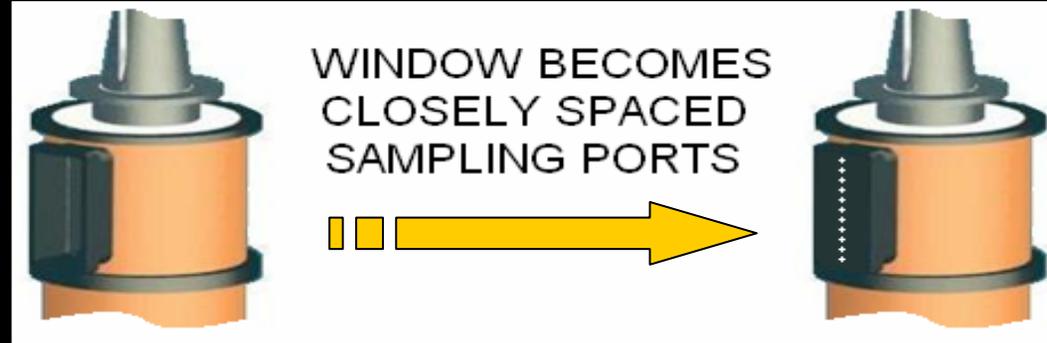


# Planned Experiments (Subject to change)

- Devolatilization:

- ~1cm resolution gas sampling near burner

- $O_2$
- $NO_x$
- HCN,  $NH_3$ , CO



- Doping of reactants ( $CO_2$ ) with  $NO_x$
- Vary  $\Phi$ ,  $O_2/CO_2$  ratios, depth of staging
- OEC?



# Planned Experiments (Subject to change)

- Corrosion:
  - Staged combustion of 3 coals
    - Illinois 6 (High Cl, S, K, Med Na)
    - PRB (High Na, Low Cl, S)
    - Pittsburgh 8 (High S, K, Med Cl, Low Na)
  - Mineral analysis of fly ash
  - SEM analysis of simulated superheater deposits



# Acknowledgements

- We would like to thank the DOE, UCR program for the funding to do this work
- Air-Liquide for funding and technical support



# Questions and Suggestions

