

# Condensed-phase Equilibrium for Ash-forming Fuels

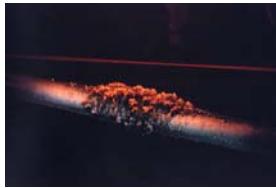


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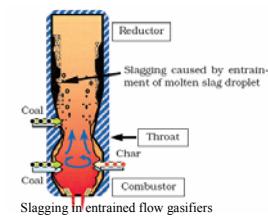
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## Background

- Serious ash deposition/sludging dominates design and operation of thermal processors with ash-forming fuels.
- Phase equilibria and viscosity play a key role in deposit properties.
- Fusion temperature of ash/slags varies with composition.
- Thermodynamic models calculate slag melting points and compositions.



Ash deposition on the surface of heat exchangers



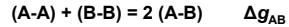
Slagging in entrained flow gasifiers

## Objectives

- Develop a thermodynamic model to correlate/predict high-temperature phase diagrams.
- Validate the model using available experimental data

## Modified Quasi-chemical Model

In a binary system composed of components A and B, the mixing Gibbs energy change can be accounted for by a quasi-chemical reaction:



The Total Gibbs energy of the system is:

$$G = (x_A g_A^o + x_B g_B^o) - T\Delta S^{\text{config}} + (n_{AB}/2)\Delta g_{AB}$$

$G$ : total Gibbs energy of the solution

$T$ : temperature

$x_i$ : mole fraction of the components

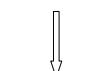
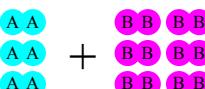
$g^o$ : Gibbs energy of the pure component

$\Delta S^{\text{config}}$ : configurational entropy

$n_{AB}$ : number of AB pairs in the solution

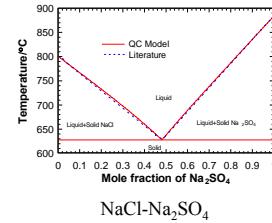
$\Delta g_{AB}$ : nonconfigurational gibbs energy change

The  $\Delta g_{AB}$  term accounts for the Gibbs energy change due to the quasi-chemical reaction and is usually expressed as a polynomial function of  $x_i$  or mole fractions of A-A and/or B-B pairs. The coefficients of the polynomial function result from optimizing phase equilibrium and/or heat of mixing data.

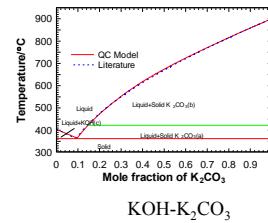


## Results

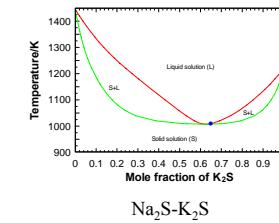
### Binary Inorganic Salt Systems



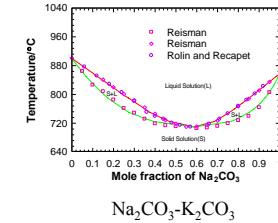
NaCl-Na<sub>2</sub>SO<sub>4</sub>



KOH-K<sub>2</sub>CO<sub>3</sub>

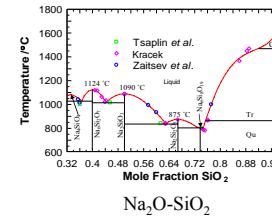


Na<sub>2</sub>S-K<sub>2</sub>S

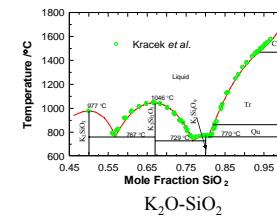


Na<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub>

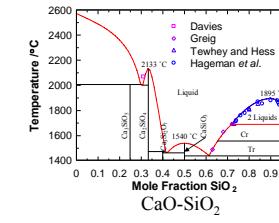
### Silicate Systems



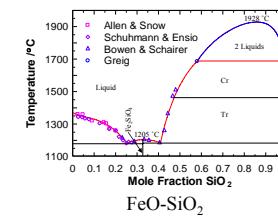
Na<sub>2</sub>O-SiO<sub>2</sub>



K<sub>2</sub>O-SiO<sub>2</sub>



CaO-SiO<sub>2</sub>



FeO-SiO<sub>2</sub>

### Melting Points (MP) of Intermediate Compounds and Eutectic Points (EP) in Silicate Systems

Component	Calculated MP (°C)	Literature MP (°C)
K <sub>2</sub> SiO <sub>3</sub>	977	976–977
K <sub>2</sub> Si <sub>2</sub> O <sub>5</sub>	1046	1045–1046
K <sub>2</sub> Si <sub>3</sub> O <sub>9</sub>	770	769–771
Na <sub>2</sub> SiO <sub>3</sub>	1090	1090–1100
Na <sub>2</sub> Si <sub>2</sub> O <sub>5</sub>	875	875
Na <sub>2</sub> SiO <sub>4</sub>	1085	1085
Na <sub>2</sub> Si <sub>2</sub> O <sub>7</sub>	1124	1124
Ca <sub>2</sub> SiO <sub>4</sub>	–	1800–2149
Ca <sub>2</sub> SiO <sub>4</sub>	2133	2130–2145
CaSiO <sub>3</sub>	1540	1540–1544

Type	Calculated EP		Literature EP	
$T$ (°C)	$x(\text{SiO}_2)$	$T$ (°C)	$x(\text{SiO}_2)$	
K <sub>2</sub> SiO <sub>3</sub> -K <sub>2</sub> Si <sub>2</sub> O <sub>5</sub>	767	0.569	780–781	0.567
K <sub>2</sub> Si <sub>2</sub> O <sub>5</sub> -K <sub>2</sub> Si <sub>3</sub> O <sub>9</sub>	729	0.767	743	0.764–0.766
K <sub>2</sub> Si <sub>3</sub> O <sub>9</sub> -SiO <sub>2</sub> (Qu)	770	0.807	770	0.805
Na <sub>2</sub> SiO <sub>3</sub> -Na <sub>2</sub> Si <sub>2</sub> O <sub>5</sub>	1029	0.367	1002	0.361
Na <sub>2</sub> Si <sub>2</sub> O <sub>5</sub> -Na <sub>2</sub> Si <sub>3</sub> O <sub>9</sub>	1015	0.442	1016	0.455
Na <sub>2</sub> SiO <sub>3</sub> -Na <sub>2</sub> SiO <sub>4</sub>	839	0.623	841–847	0.614–0.63
Na <sub>2</sub> SiO <sub>3</sub> -SiO <sub>2</sub> (Qu)	804	0.747	794–799	0.742
Ca <sub>2</sub> SiO <sub>4</sub> -Ca <sub>2</sub> SiO <sub>4</sub>	2023	0.295	2057–2060	0.273–0.30
Ca <sub>2</sub> Si <sub>2</sub> O <sub>7</sub> -CaSiO <sub>3</sub>	1467	0.422	1450–1460	0.42–0.445
CaSiO <sub>3</sub> -SiO <sub>2</sub> (Tr)	1441	0.615	1441–1444	0.61–0.635

## Conclusions

- A modified quasi-chemical model taken from the literature has been used to correlate phase diagrams of inorganic salts and silicates.
- The model has been validated using several binary systems.
- Thermodynamic properties of many pure compounds have been collected, approximated, or optimized.
- The results of the model in correlating low-order phases can be used in extrapolations to multi-component systems.

**Acknowledgement** This work is financially supported by industrial sponsors and is part of the ash deposition project in Brigham Young University

Many binary salt and silicate phase diagrams have been modeled and are available from the ash deposition group at Brigham Young University: NaCl-Na<sub>2</sub>CO<sub>3</sub>, KCl-K<sub>2</sub>CO<sub>3</sub>, NaCl-Na<sub>2</sub>SO<sub>4</sub>, KCl-K<sub>2</sub>SO<sub>4</sub>, K<sub>2</sub>CO<sub>3</sub>-KOH, KCl-MgCl<sub>2</sub>, Na<sub>2</sub>O-SiO<sub>2</sub>, CaO-SiO<sub>2</sub>, Al<sub>2</sub>O<sub>3</sub>-SiO<sub>2</sub>, FeO-SiO<sub>2</sub>, Na<sub>2</sub>S-K<sub>2</sub>S, etc.

## Future Work

- Expand the model validation to ternary and higher-order systems
- Collect and develop a database for the pure component properties and binary interaction parameters that can be used for multicomponent systems.
- Combine the phase equilibrium results with viscosity models to predict viscosities of slags in multi-component phases.

