

Effects of Particle Shape and Size on Biomass Reactivity

Hong Lu, Luke Werrett, Mark Vickers, Todd Gunderson Larry L. Baxter

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Introduction



- More cofiring boilers are used in power plants
- Biomass particle shape and size
 - Irregular shapes: typically flake-like and cylinder-like (aspect ratios 2-15)
 - Larger size (1~6 mm)
- Biomass particle surface area
 - Surface area/volume essential to heat, mass, and momentum transfer
 - Sphere is extreme case (lowest surface area to volume ratio of all shapes)
- Comprehensive particle model needed for biomass combustion, which may not be simply approximated by isothermal spheres



Objectives



- Establish a biomass combustion database for particles with different shapes and sizes
 - Collecting experimental data for particles with varying shapes and sizes: mass loss, particle volume, surface area, shape, and surface temperature as functions of residence time.
- Develop a comprehensive biomass particle combustion model
 - This model should be capable of simulating combustion behaviors of biomass particles with any shape and size.



Samples - sawdust







flake-like



cylinder-like

near-spherical



Samples - poplar







Methods - entrained flow reactor



- •0.43m high
- •50mm in diameter
- •Electrically heated up to 1600 K
- Feeding rate as lowas 0.7 gm/hr





Methods-particle reactor & imaging system





* The three viewports are in three orthogonal direction



Method –shape reconstruction





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Method – shape reconstruction

- Image edge detection walking algorithm ۲
- Image alignment and surface points interpolation IDW
- Errors for both Volume and surface area are < 10%













Reconstructed 3D sawdust particle shape



ZY



Method – temperature measurement



•Thermocouples and cameras were used to measure particle temperature

•Temperature measurement and calculation by color-bands method will be discussed by Dr. Tree in detail









Method- temperature mapping















Physical model





- Drying Model
 - Liquid phase (free water, bound water) diffusion in the particle
 - Internal and external evaporation
 - Vapor phase diffusion and convection

$$\frac{\partial \rho_m}{\partial t} = \frac{1}{r^n} \frac{\partial}{\partial r} \left(r^n D_{\text{eff},m} \frac{\partial \rho_m}{\partial r} \right) + S_m$$

where, $D_{\text{eff},m} = f D_{\text{eff},m,f} + b D_{\text{eff},m,b}$
 $S_m = -S_a h_{m,pore} (\rho_{v,sat} - \rho_v),$

 s_a is the liquid/gas inferface area in the particle.

$$\frac{\partial}{\partial t}\varepsilon\rho_{g}Y_{v} + \frac{1}{r^{n}}\frac{\partial}{\partial r}(r^{n}\varepsilon\rho_{g}Y_{v}u) = \frac{1}{r^{n}}\frac{\partial}{\partial r}(r^{n}\varepsilon D_{eff,v}\rho_{g}\frac{\partial Y_{v}}{\partial r}) + S_{v}$$

where, $S_{v} = s_{a}h_{m,p}(\rho_{v,sat} - \rho_{v})$





Pyrolysis model

$$\frac{\partial \rho_B}{\partial t} = -(r1 + r2 + r3)$$



$$\frac{\partial}{\partial t}\varepsilon\rho_{g}Y_{i} + \frac{1}{r^{n}}\frac{\partial}{\partial r}(r^{n}\varepsilon\rho_{g}Y_{i}u) = \frac{1}{r^{n}}\frac{\partial}{\partial r}(r^{n}\varepsilon D_{\text{eff},i}\rho_{g}\frac{\partial Y_{i}}{\partial r}) + S_{i}$$

where i = T for tar, G for light gas, and I for inert gas

$$\frac{\partial}{\partial t}\varepsilon\rho_g + \frac{1}{r^n}\frac{\partial}{\partial r}(r^n\varepsilon\rho_g u) = S_g$$

n is shape factor: 2-sphere, 1-cylinder, 0-slab







Char oxidation and gasification model

- C+ $\frac{1}{2}$ O2 \rightarrow CO (6)
- $C + CO2 \rightarrow 2 CO$ (7)
- C + H2O \rightarrow H2 + CO (8)
- H2+ $\frac{1}{2}$ O2 \rightarrow H2O (9)
- $CO + \frac{1}{2}O2 \to CO2$ (10)

$$\frac{\partial \rho_{c}}{\partial t} = r3 + r5 - (r6 + r7 + r8)$$
$$\frac{\partial}{\partial t} \varepsilon \rho_{g} Y_{i} + \frac{1}{r^{n}} \frac{\partial}{\partial r} (r^{n} \varepsilon \rho_{g} Y_{i} u) = \frac{1}{r^{n}} \frac{\partial}{\partial r} (r^{n} \varepsilon D_{\text{eff}, i} \rho_{g} \frac{\partial Y_{i}}{\partial r}) + S_{i}$$

where i = CO2, CO, H2, O2





Energy balance and momentum balance

$$\frac{\partial}{\partial t} \left[\left(\rho_B \hat{H}_B + \rho_C \hat{H}_C + \rho_M \hat{H}_M \right) + \varepsilon \rho_g \left(\sum_i Y_i \hat{H}_i \right) \right] \\ + \frac{1}{r^n} \frac{\partial}{\partial r} \left[r^n \varepsilon \rho_g u \left(\sum_i Y_i \hat{H}_i \right) \right] = \frac{1}{r^n} \frac{\partial}{\partial r} (r^n k_{eff} \frac{\partial T}{\partial r}) \\ + \frac{1}{r^n} \frac{\partial}{\partial r} \left[r^n \rho_g \varepsilon \left(\sum_i D_{eff,i} \frac{\partial Y_i}{\partial r} \hat{H}_i \right) + r^n D_{eff,M} \frac{\partial \rho_M}{\partial r} \hat{H}_M \right] \\ U = -\frac{\eta}{\mu} \frac{\partial P}{\partial r}$$

Equations solved by control volume method





• Pyrolysis Mass Loss History –sawdust with various shapes







•Pyrolysis conversion time comparison





•Drying and Pyrolysis (d=11.5 mm near spherical poplar)





•Pyrolysis (d=11.5 mm near spherical poplar)







•Combustion (near spherical poplar in air)





•Pyrolysis conversion time comparison





Conclusions



- A biomass particle combustion model has been developed for fuels have irregular shapes
- Particle shape and size strongly affect conversion time during pyrolysis, consistent with model results
- Near spherical biomass particle was found to lose mass most slowly during pyrolysis, also consistent with theory
- Shape effects impact particle reactions in substantial ways when particles are large (> 300 µm equivalent diameter)
- Irregular particle shape can be reconstructed using three images
- Particle surface temperature can be calculated by the color-band method and mapped to the 3D particle model

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